

Chapter 7 Phase equilibrium in one component system

$$1. \quad * \text{ Thermodynamic equil. } \begin{cases} \text{Thermal equilibrium} & T_\alpha = T_\beta \\ \text{Mechanical equilibrium} & P_\alpha = P_\beta \\ \text{Chemical equilibrium} & \mu_\alpha = \mu_\beta \end{cases}$$

* At constant T, P. equil. $\Leftrightarrow G' = G_{\min}, \quad dG' = 0$

* $G = H - TS$

For constant P = 1 atm with H(T), S(T) known.

$$G(T) \text{ can be calculated for } \begin{cases} \text{one component} \\ \text{closed system} \\ \text{single phase} \end{cases}$$

$G_\alpha(T)$ for different phases \Rightarrow stable (equilibrium) phase at specific T is the lowest G_α phase.

2. $G(T), \Delta G(T)$ at constant P = 1 atm

Consider: P = 1 atm, T = 273 K. $H_2O_{(s)} \rightarrow H_2O_{(l)}$

* Adding heat, if (ice + water) coexist, only ratio of ice/water changes, total Gibbs free energy G' remains constant.

$$\Delta G = G_{H_2O(l)} - G_{H_2O(s)} = 0$$

i.e. $G_{H_2O(l)} = G_{H_2O(s)}$

Assume: $\begin{cases} H_2O_{(s)} \text{ has } n_{H_2O(s)} \text{ moles} \\ H_2O_{(l)} \text{ has } n_{H_2O(l)} \text{ moles} \end{cases}$

$$\therefore G' = n_{H_2O(s)} \cdot G_{H_2O(s)} + n_{H_2O(l)} \cdot G_{H_2O(l)} \dots\dots\dots *1$$

$$= [n_{H_2O(s)} + n_{H_2O(l)}] \cdot G_{H_2O(s)}$$

$\therefore (n_{H_2O(s)} + n_{H_2O(l)})$ is fixed. (closed system)

When $\frac{n_{H_2O(s)}}{n_{H_2O(l)}}$ is changed. G' does not change.

* $dG = -SdT + VdP + \sum \mu_i dn_i$ constant T, P.

$$\therefore G'_{T,P} = \int dG = \sum \int \mu_i dn_i$$

$$\therefore G' = \mu_{H_2O(s)} \cdot n_{H_2O(s)} + \mu_{H_2O(l)} \cdot n_{H_2O(l)} \dots\dots\dots *2$$

c.p. (*1)(*2) $\therefore \mu_{H_2O} = G_{H_2O}, \quad \mu_i = G_i$

Chemical potential \Leftrightarrow molar Gibbs free energy.

Definition:
$$\mu_i \equiv \left(\frac{\partial G'}{\partial n_i} \right)_{n_j, T, P} = \bar{G}_i$$

For one component system (i), $n_j = 0$

Adding one mole of i, i.e. $\Delta n_i = 1$

$\therefore \Delta G' = G_i = \mu_i$

* $P = 1 \text{ atm}, T < 0^\circ\text{C}.$ $G_{\text{H}_2\text{O}(s)} < G_{\text{H}_2\text{O}(l)}$

$\therefore \Delta G = G_{\text{H}_2\text{O}(l)} - G_{\text{H}_2\text{O}(s)} > 0$ ice is stable.

$T > 0^\circ\text{C}.$ $G_{\text{H}_2\text{O}(s)} > G_{\text{H}_2\text{O}(l)}$ water is stable.

$G_{(s)}(T) = ?$ $G_{(l)} = ? \Leftrightarrow C_{p(s)}, C_{p(l)}$

* H_2O $\left\{ \begin{array}{l} C_{p(s)} = 38 \text{ J/k} \cdot \text{mole} \\ C_{p(l)} = 75.44 \text{ J/k} \cdot \text{mole} \\ \text{at } 298\text{K} \quad S_{(s)} = 44.77 \text{ J/k} \cdot \text{mole} \quad H_{(s)} = -6944 \text{ J/mole} \\ \quad \quad \quad S_{(l)} = 70.08 \text{ J/k} \cdot \text{mole} \quad H_{(l)} \equiv 0 \\ T_m = 0^\circ\text{C} = 273\text{K}, \quad \Delta H_{s \rightarrow l} = \Delta H_m = 6008 \text{ J/mole} \end{array} \right.$

$H(T) = \int_{298}^T C_p \cdot dT + H_{298}$

$S(T) = \int_{298}^T \frac{C_p}{T} \cdot dT + S_{298}$

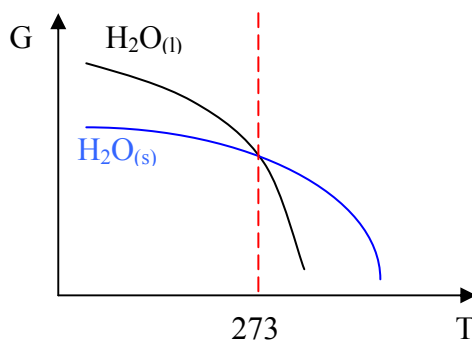
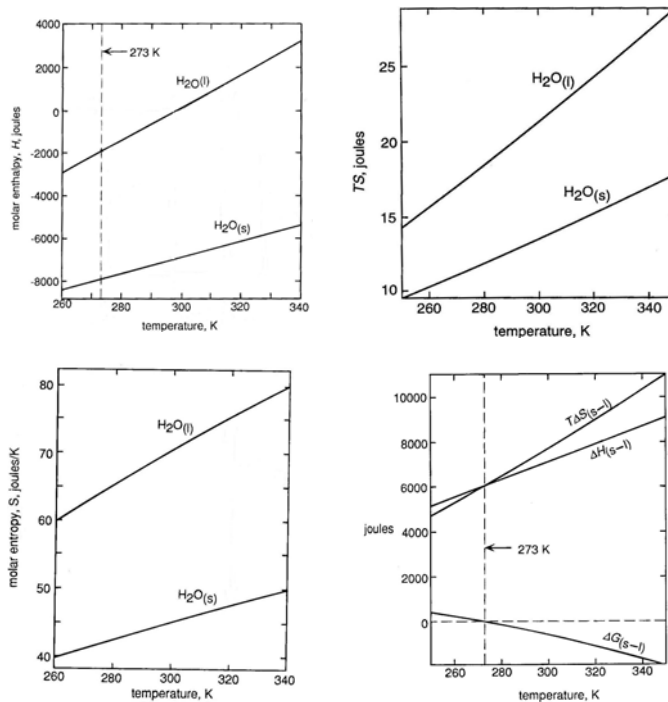
$\therefore G(T) = H(T) - T \cdot S(T)$

$\therefore \begin{cases} G_{(s)} = H_{(s)} - T \cdot S_{(s)} \\ G_{(l)} = H_{(l)} - T \cdot S_{(l)} \end{cases}$

$\Delta G_{s \rightarrow l} = G_l - G_s = [H_{(l)} - H_{(s)}] - T[S_{(l)} - S_{(s)}]$

$\Delta G_{s \rightarrow l} = \Delta H_{s \rightarrow l} - T \cdot \Delta S_{s \rightarrow l}$

when $\begin{cases} T = T_m & \Delta G_{s \rightarrow l} = 0 & \Delta H_m = T_m \Delta S_m \\ T < T_m & \Delta G_{s \rightarrow l} > 0 \\ T > T_m & \Delta G_{s \rightarrow l} < 0 \end{cases}$



Note: $H_{(l)} > H_{(s)}$

$$S_{(l)} > S_{(s)}$$

$$\Delta H = H_{(l)} - H_{(s)} > 0$$

$$\Delta S = S_{(l)} - S_{(s)} > 0 \quad \text{but } \Delta H > \Delta S$$

$$\Delta G = \Delta H - T\Delta S \quad \begin{cases} \text{low } T : \Delta H \text{ dominates} \\ \text{high } T : -\Delta S \text{ dominates} \end{cases}$$

$$\therefore \text{low } T : \Delta G > 0, \quad \text{high } T : \Delta G < 0$$

$$\text{at } T = T_m, \quad \Delta G = 0$$

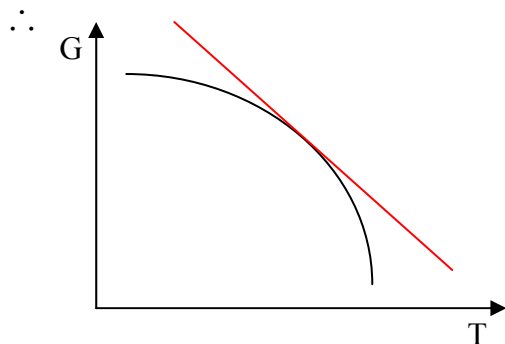
* Shape of G(T), ΔG(T) curves (P = 1 atm)

① single phase:

$$\left(\frac{\partial G}{\partial T}\right)_P = -S < 0$$

$$\left(\frac{\partial^2 G}{\partial T^2}\right)_P = -\left(\frac{\partial S}{\partial T}\right)_P = -\frac{C_P}{T} < 0$$

$\because T > 0, S > 0, C_p > 0$



② Phase transition: (melting)

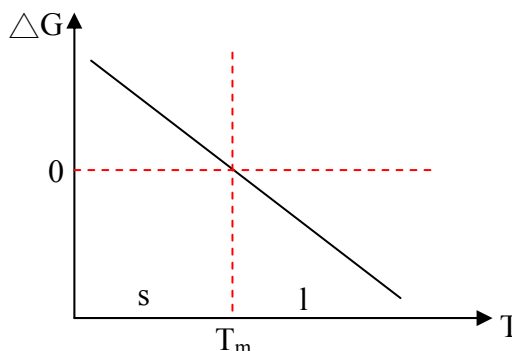
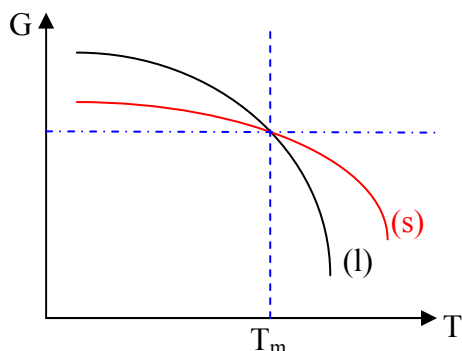
$$\Delta G = G_{(l)} - G_{(s)}$$

$$\left(\frac{\partial \Delta G}{\partial T}\right)_P = -\Delta S = -(S_{(l)} - S_{(s)}) < 0$$

$$\left(\frac{\partial^2 \Delta G}{\partial T^2}\right)_P = -\left(\frac{\partial \Delta S}{\partial T}\right)_P \cong -\frac{\Delta C_p}{T} \approx -\frac{[C_{p(l)} - C_{p(s)}]}{T} \approx 0$$

* ΔC_p indep. of T

* Richards' $\Delta S_m \approx 8.4 \text{ J/k} \cdot \text{mole}$



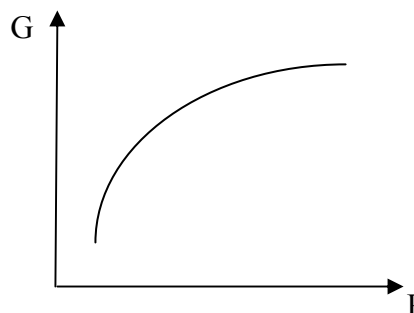
3. $G(P), \Delta G(P)$ at constant T.

* shape of curves

① Homogeneous single phase

$$\left(\frac{\partial G}{\partial P}\right)_T = V > 0$$

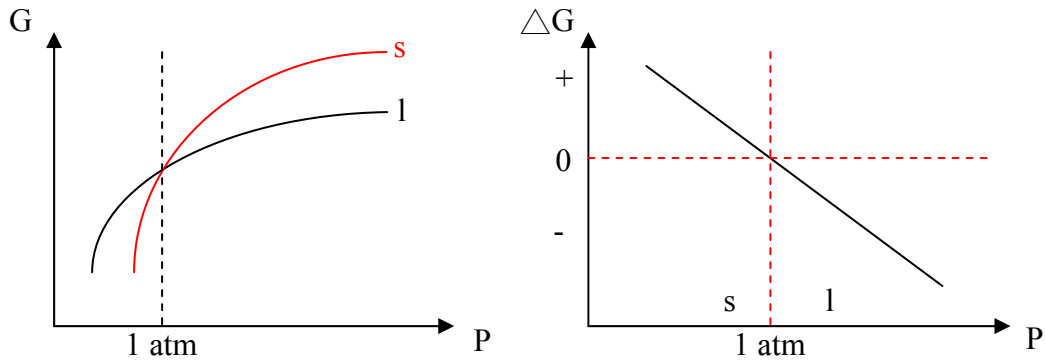
$$\left(\frac{\partial^2 G}{\partial P^2}\right)_T = \left(\frac{\partial V}{\partial P}\right)_T = -\beta V < 0$$



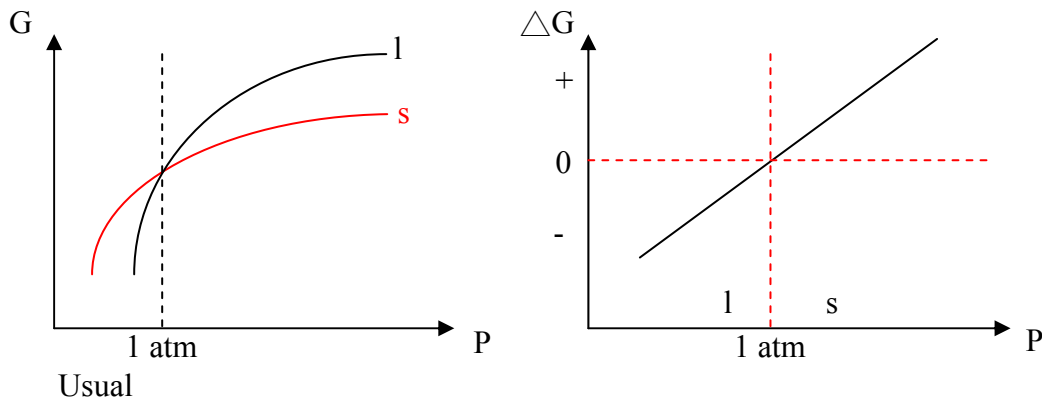
② Phase transition (melting)

$$\left(\frac{\partial \Delta G}{\partial P}\right)_T = \Delta V = V_{(l)} - V_{(s)} \begin{cases} H_2O, \Delta V < 0 \\ \text{Usual: } \Delta V > 0 \end{cases}$$

$$\left(\frac{\partial^2 \Delta G}{\partial P^2}\right)_T = \left(\frac{\partial \Delta V}{\partial P}\right)_T \cong -[\beta_l V_l - \beta_s V_s] \begin{cases} > 0 \\ < 0 \end{cases}$$



For H₂O, ∵ ΔV > 0, P ↑ ⇔ ΔG ↓ ⇔ liquid water is stable.



Usual

4. Phase equilibrium between solid and liquid. $T_{s>l}(P) = ?$ $T_m(P) = ?$

Equilibrium. $G_{(l)} = G_{(s)}$ ∵ $dG_{(l)} = dG_{(s)}$

$$\begin{aligned} \therefore \begin{cases} dG_{(l)} = -S_{(l)}dT + V_{(l)}dP \\ dG_{(s)} = -S_{(s)}dT + V_{(s)}dP \end{cases} \\ \therefore -S_{(l)}dT + V_{(l)}dP = -S_{(s)}dT + V_{(s)}dP \end{aligned}$$

$$\left(\frac{dP}{dT}\right)_{eq.} = \frac{S_{(l)} - S_{(s)}}{V_{(l)} - V_{(s)}} = \frac{\Delta S_{(s \rightarrow l)}}{\Delta V_{(s \rightarrow l)}}$$

and ∵ $\Delta G = 0 \Rightarrow \Delta H = T \cdot \Delta S$

$$\therefore \boxed{\left(\frac{dP}{dT}\right)_{eq.} = \frac{\Delta H}{T \cdot \Delta V}} \quad \text{Clapeyron eq.}$$

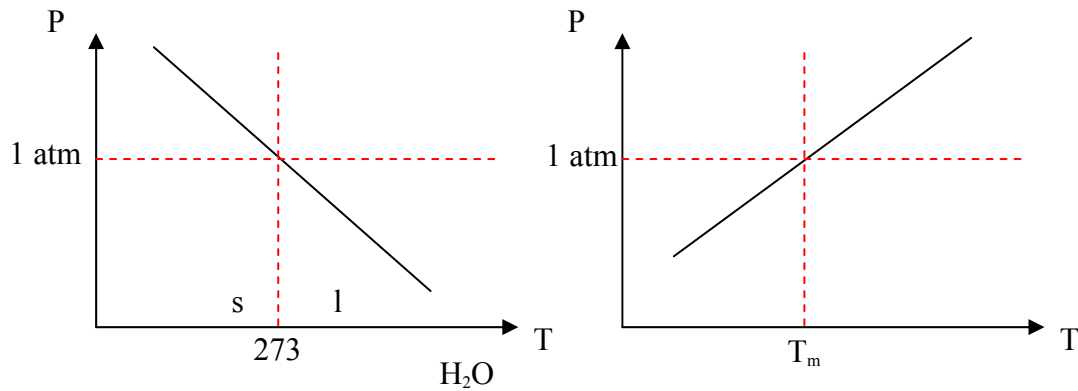
Ex: H₂O: s-> l

$$\left. \begin{aligned} \Delta H_{sl} > 0 \\ \Delta V_{sl} < 0 \end{aligned} \right\} \left(\frac{dP}{dT}\right) < 0$$

$$P \uparrow \Rightarrow T_{sl} \downarrow$$

If R.T. = -1° C under skate, (P ↑), $T_{sl} \approx -3^\circ \text{C}$, ice melts
 ⇒ water is lubricant.

Most materials, $\Delta V_{sl} > 0$. $\therefore P \uparrow \Rightarrow T_m \uparrow$



* Note: 3D diagram G-T-P (phase) Fig. 7-3(D) (or 7-8(G))

$$G(T,P) = H(T,P) - T \times S(T,P)$$

Projection of $G_{(s)} = G_{(l)}$ curve on (T-P) plane.

5. Solid (liquid) \Leftrightarrow Vapor phase equilibrium

* Equilibrium vapor pressure over solid (liquid)?

Condensed phase \rightarrow Vapor

$$\Delta V = V_{\text{vapor}} - V_{\text{cond.}} \doteq V_{\text{vapor}}$$

$$\therefore \left(\frac{dP}{dT} \right)_{eq.} = \frac{\Delta H}{T \cdot \Delta V} \approx \frac{\Delta H}{T \cdot V_{(v)}}$$

Assume ideal gas, $PV = RT$

$$\therefore \left(\frac{dP}{dT} \right)_{eq} = \frac{P\Delta H}{RT^2}$$

$$\therefore \frac{dP}{P} = \frac{\Delta H}{RT^2} dT$$

$$\boxed{d \ln P = \frac{\Delta H}{RT^2} dT} \quad \text{Clausius-Clapeyron eq. (ideal gas)}$$

①

If $\Delta H \neq f(T)$, i.e. $C_p(\text{vapor}) = C_p(\text{cond.})$

$$\therefore \Delta C_p = 0$$

$$\therefore \ln P = -\frac{\Delta H}{RT} + \text{const.}$$

②

If $\Delta C_p = \text{constant} \neq f(T)$

$$\therefore \Delta H(T_2) = \Delta H(T_1) + \int_{T_1}^{T_2} \Delta C_p dT$$

$$\begin{aligned}\therefore \Delta H(T) &= \Delta H_{298} + \int_{298}^T \Delta C_p dT \\ &= \Delta H_{298} + \Delta C_p (T - 298) \\ &= (\Delta H_{298} - 298 \cdot \Delta C_p) + T \cdot \Delta C_p \\ \therefore \int d \ln P &= \int \frac{\Delta H_{298} - 298 \cdot \Delta C_p}{RT^2} \cdot dT + \int \frac{\Delta C_p}{RT} \cdot dT\end{aligned}$$

Then $\boxed{\ln P = \frac{A}{T} + B \ln T + C}$

③

If T_b , ΔH_b , $C_{p(l)}$, $C_{p(v)}$ are known, then saturated vapor pressure $P(T)$ can be calculated.

Note: normal boiling temperature: T_b . At $T = T_b$, $P = 1 \text{ atm}$.

e.g. $C_{p,H_2O(l)} = 75.44 \text{ J/k}$

$$C_{p,H_2O(v)} = 30 + (10.7 \times 10^{-3})T + (0.33 \times 10^{-5})T^2 \quad \text{J/k}$$

$$T_b = 100^\circ\text{C} = 373 \text{ k} \quad \Delta H_b = 41090 \quad \text{J/mole}$$

$$\therefore d \ln P = \frac{\Delta H_{\text{evap}}}{RT^2} dT \dots \dots \dots *$$

$$\therefore \Delta H_{\text{evap}}(T) = \Delta H_{\text{evap}}(373) + \int_{373}^T \Delta C_p(l \rightarrow v) dT$$

$$\left\{ \begin{aligned} \Delta H_{\text{evap}}(373) &= \Delta H_b \\ \Delta C_p(l \rightarrow v) &= C_{p,H_2O(v)} - C_{p,H_2O(l)} \end{aligned} \right.$$

$$\Rightarrow \Delta H_{\text{evap}}(T) = 41090 + \int_{373}^T [-45.44 + (10.7 \times 10^{-3}) \times T + (0.33 \times 10^{-5}) \times T^2] dT$$

$$= 41090 + (-45.44)(T - 373) + \frac{10.7 \times 10^{-3}}{2} (T^2 - 373^2)$$

$$- (0.33 \times 10^{-5}) \left(\frac{1}{T} - \frac{1}{373} \right)$$

$$= 58872 - 45.44T + (5.35 \times 10^{-3}) \times T^{-2} - \frac{0.33 \times 10^{-5}}{T} \quad \text{J}$$

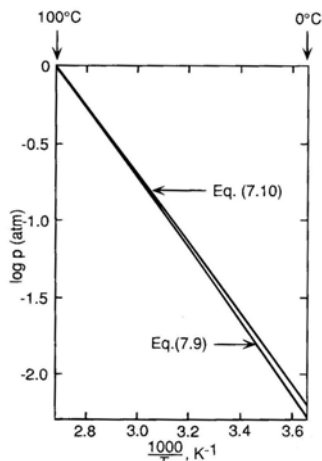
From the eq. *, we get

$$\Rightarrow \ln P = -\frac{58872}{RT} - \frac{45.44 \ln T}{R} + \frac{(5.35 \times 10^{-3}) \times T}{R} + \frac{0.33 \times 10^{-5}}{2RT^2} + \text{const.}$$

$$\therefore T = 373 \text{ k}, \quad P = 1 \text{ atm}, \quad \therefore \text{const.} = 51.1$$

$$\log P(\text{atm}) = -\frac{58872}{2.303RT} - \frac{45.44 \log T}{R} + \frac{(5.35 \times 10^{-3})T}{2.303R} + \frac{0.33 \times 10^{-5}}{2.303 \times 2RT^2} + \frac{51.1}{2.303}$$

$$\text{Experimental data: } \log P(\text{atm}) = -\frac{2900}{T} - 4.65 \log T + 19.732$$



6. Phase diagram in one component system

On a P-T space, draw curves for:

s→l, l→v and s→v equilibrium

From $\left(\frac{dP}{dT}\right)_{eq} = \frac{\Delta H}{T \cdot \Delta V}$, obtain $P(T)$ curve.

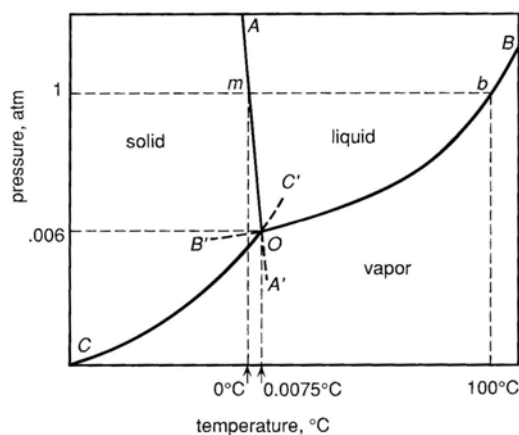
For s ↔ l: $\Delta H(T) = \Delta H_m + \int_{T_m}^T [C_{p(l)} - C_{p(s)}] \cdot dT$

* if $\Delta H(T)$ is indep. of T, then $dP = \frac{\Delta H}{\Delta V} \frac{dT}{T}$

$$\therefore P = \frac{\Delta H}{\Delta V} \cdot \ln T + const.$$

Normal melting T_{mp} , $P = 1 \text{ atm}$, $T = T_m \Rightarrow const.$

$$\text{For } \left. \begin{matrix} l \leftrightarrow v \\ s \leftrightarrow v \end{matrix} \right\} \log P = \frac{A}{T} + B \log T + C$$



For H₂O

O: triple point

At triple point $\Leftrightarrow P(s \rightarrow v) = P(s \rightarrow l) = P_{\text{triple}}$

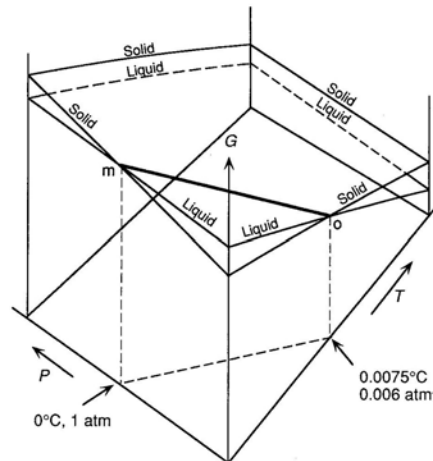
∴ ① if $P(s \rightarrow v)(T)$, and $P(l \rightarrow v)(T)$ are known,

T_t can be calculated.

$$\begin{cases} \log P_{sv} = \frac{A_s}{T} + B_s \cdot \log T + C_s \\ \log P_{lv} = \frac{A_l}{T} + B_l \cdot \log T + C_l \end{cases}$$

$$\therefore \frac{A_s}{T_t} + B_s \cdot \log T_t + C_s = \frac{A_l}{T_t} + B_l \cdot \log T_t + C_l$$

* 3D diagram G-T-P



* According Gibbs Phase Rule: $F = C + 2 - P$

$$\begin{cases} F : \text{number of degree of freedom} \\ C : \text{number of component} \\ P : \text{number of phase} \\ 2 : T, P \text{ variables} \end{cases}$$

$$\text{For } = 3 - P: \begin{cases} \text{single phase region} \Rightarrow F = 2 \text{ (area)} \\ \text{two phase equil.} \Rightarrow F = 1 \text{ (line)} \\ \text{three phase equil.} \Rightarrow F = 0 \text{ (point)} \end{cases}$$

* G-T curves at different P (see Fig. 7.12)

* G-P curves at different T (see Fig. 7.13)

7. Solid-solid equilibria

* Allotropy: elements exist in more than one crystal form.

e.g. Fe: α , γ , δ

* Polymorphism: compounds exist in more than one crystal forms.

e.g. ZrO_2 : monoclinic, tetragonal, cubic, (liquid)

* $\text{Solid}(\alpha) \rightleftharpoons \text{Solid}(\beta)$

$$\left(\frac{dP}{dT}\right)_{eq} = \frac{\Delta H}{T \cdot \Delta V} = \frac{\Delta S}{\Delta V}$$

e.g. $\alpha - Fe(BCC) \rightarrow \gamma - Fe(FCC) \rightarrow \delta - Fe(BCC)$

$$\begin{cases} V(\alpha - Fe) > V(\gamma - Fe) & (\Delta V_{\alpha\gamma} < 0) \quad (\because \rho_{FCC} > \rho_{BCC}) \\ V(\gamma - Fe) < V(\delta - Fe) & (\Delta V_{\gamma\delta} > 0) \end{cases}$$

$$\therefore \Delta H > 0$$

$$\therefore \left(\frac{dP}{dT}\right)_{\alpha\gamma} < 0, \quad \left(\frac{dP}{dT}\right)_{\gamma\delta} > 0$$

For phase transition between condensed phases,

$$\left(\frac{\Delta S}{\Delta V}\right) \approx \text{const.} \quad (\text{insensitive to } T, P)$$

$$\therefore P \cong \left(\frac{\Delta S}{\Delta V}\right) \cdot T + \text{const.}$$

Ex1. NaF

$$\left\{ \begin{array}{l} s \leftrightarrow g : \ln P(\text{atm}) = -\left(\frac{34450}{T}\right) - 2.01 \times \ln T + 33.74 \dots \dots \dots (1) \\ l \leftrightarrow g : \ln P(\text{atm}) = -\left(\frac{31090}{T}\right) - 2.52 \times \ln T + 34.66 \dots \dots \dots (2) \end{array} \right.$$

$$\left\{ \begin{array}{l} l \leftrightarrow g : \ln P(\text{atm}) = -\left(\frac{31090}{T}\right) - 2.52 \times \ln T + 34.66 \dots \dots \dots (2) \end{array} \right.$$

$$Q: (a) T_b = ? \quad (b) T_t = ? \quad P_t = ?$$

$$(c) \Delta H_b = ? \quad (d) \text{When } T = T_t \quad \Delta H_{s,l}(T_t)$$

$$(e) \Delta C_p = C_{p(l)} - C_{p(s)} = ?$$

Solu:

$$(a) T = T_b, \quad P = 1 \text{ atm}$$

$$\text{from (2)} \Leftrightarrow \ln 1 = 0 = -\frac{31090}{T_b} - 2.52 \ln T_b + 34.66$$

$$\therefore T_b = 2006 \text{ K}$$

$$(b) \text{At triple point: (1) = (2)}$$

$$\therefore -\frac{34450}{T_t} - 2.01 \times \ln T_t + 33.74 = -\frac{31090}{T_t} - 2.52 \times \ln T_t + 34.66$$

$$\therefore T_t = 1239 \text{ K}$$

$$P_t = \exp\left(-\frac{34450}{1239} - 2.01 \cdot \ln 1239 + 33.74\right) = 2.29 \times 10^{-4} \text{ atm}$$

$$(c) \because d \ln P = \frac{\Delta H}{RT^2} \cdot dT, \quad \therefore \Delta H = RT^2 \left(\frac{d \ln P}{dT}\right)$$

$$l \rightarrow v: \ln P = -\frac{31090}{T} - 2.52 \cdot \ln T + 34.66$$

$$\therefore \Delta H_g = RT^2 \left[\frac{31090}{T^2} - 2.52 \cdot \frac{1}{T} \right] = 258500 - 20.95T$$

$$T = T_b = 2006\text{k}, \quad \Delta H_{l \rightarrow g} = \Delta H_b = 216500 \text{ J}$$

$$\begin{aligned} \text{(d)} \quad \Delta H_{sl} &= H_l - H_s = H_l - H_g + H_g - H_s \\ &= -(H_g - H_l) + (H_g - H_s) = \Delta H_{s \rightarrow g} - \Delta H_{l \rightarrow g} \end{aligned}$$

$$\Delta H_{s \rightarrow g} = RT^2 \cdot \left(\frac{d \ln P_{sg}}{dT} \right) = 286400 - 16.71 \cdot T$$

$$\therefore \Delta H_{sl} = \Delta H_{s \rightarrow g} - \Delta H_{l \rightarrow g} = 27900 + 4.24 \times T$$

$$T = T_t = 1239\text{k}, \quad \Delta H_{sl} = 33150 \text{ J}$$

$$\text{(e)} \quad \Delta C_{p(s \rightarrow l)} = \frac{d \cdot \Delta H_{s \rightarrow l}}{dT} = 4.24 \text{ J/k} \cdot \text{mole}$$

EX. 2: Carbon (Graphite) \rightarrow Diamond $P = ?$

$$T = 298 \text{ k}, \quad H(\text{graphite}) - H(\text{diamond}) = -1900 \text{ J}$$

$$S_{\text{graphite}} = 5.73 \text{ J/k} \cdot \text{mole}$$

$$S_{\text{diamond}} = 2.43 \text{ J/k} \cdot \text{mole}$$

$$\rho_{(\text{graphite})} = 2.22 \text{ g/cm}^3$$

$$\rho_{(\text{diamond})} = 3.515 \text{ g/cm}^3$$

Solu: graphite \rightarrow diamond at $T = 298 \text{ k}$

$$\begin{aligned} \Delta G &= \Delta H - T \cdot \Delta S \\ &= (H_d - H_g) - T \cdot (S_d - S_g) \\ &= (+1900) - 298 \times (2.43 - 5.73) = 2883 \text{ J} \end{aligned}$$

$$\left(\frac{\partial \Delta G}{\partial P} \right)_T = \Delta V, \quad \text{const.} = T$$

$$\int_{2883}^{\Delta G(P)} d(\Delta G) = \int_1^P \Delta V \cdot dP \quad \Delta V = V_d - V_g$$

$$V_{\text{diamond}} = \frac{M}{\rho_d} = \frac{12}{3.515} = 3.415 \text{ cm}^3/\text{mole}$$

$$V_{\text{graphite}} = \frac{M}{\rho_g} = \frac{12}{2.22} = 5.405 \text{ cm}^3/\text{mole}$$

$$\therefore \Delta V = -1.99 \text{ cm}^3/\text{mole}$$

$$\therefore \Delta G(P) - 2883 \cong [\Delta V(P-1)] \times \left(0.1013 \frac{\text{J}}{\text{atm} \cdot \text{cm}^3} \right)$$

$$\therefore \Delta G(P) = 2883 - 1.99 \times 0.1013 \times (P-1)$$

when $\Delta G(P) \leq 0$, phase transition occurs

$$\therefore P \geq \frac{2883}{1.99 \times 0.1013} + 1 \cong 14300 \text{ atm.}$$